

***“GEOHERMAL BINARY PLANTS:
WATER OR AIR COOLED ?”***

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Geothermal Power Plants

- Back pressure flash plants
- Condensing flash plants
- Binary plants

Cooling Options

- (water cooled condensers) & (surface water)
- (water cooled condensers) & (wet type cooling towers)
- (air cooled condensers) & (dry type cooling towers)

Carnot Efficiency

$$n = \frac{T_g - T_c}{T_g}$$

- “ T_g ”: geothermal source temperature, °K
- “ T_c ”: cooling water temperature, °K

Turbine Efficiency

$$w = n_t \cdot m \cdot (H_s - H_o)$$

$$N = n_g \cdot w$$

$$n = \frac{N}{m \cdot H_s} = \frac{n_g \cdot n_t \cdot (H_s - H_o)}{H_s}$$

- n : overall conversion efficiency
- n_g : generator efficiency
- n_t : turbine efficiency
- H_s : vapour specific enthalpy at turbine inlet
- H_o : vapour specific enthalpy at turbine outlet
- m : fluid mass flow

Water vs. Air cooled condensers

<u>property</u>	<u>water</u>	<u>air</u>
Specific heat, $\text{kJ} / \text{kg}^\circ\text{C}$	$c_{pw} = 4,19$	$c_{pa} = 1,00$
Density, kg/m^3	$\rho_w = 999$	$\rho_a = 1,2$
Volumetric Heat Capacity, $\text{kJ} / \text{m}^3^\circ\text{C}$	$VHC_w = 4182$	$VHC_a = 1,21$
Heat transfer coefficient $\text{kW} / \text{m}^2^\circ\text{C}$	$h_w = 4,84$	$h_a = 0,084$

Binary Plant Economics

- Heat Exchangers
- H.E. surface
- weight

Cooling with Surface Water

- 5 – 25 °C \Rightarrow
- lowest condensing temperature: 15-35 °C
- 970 t/h per MW_e for $\Delta T=10$ °C
- Shell & Tube Condenser
 - *cross flow, double pass*
- Plate H.E. as condenser
 - *10-20 kW_{th}/m² for $\Delta T=5$ °C*
 - *easy to clean*

Cooling with Surface Water

- Lower than ambient T in Summer
- Do not freeze in Winter
- No cooling towers
- Cogeneration possibility

Cooling with Surface Water

- Need for large water quantity
- Fouling or corrosion
- Need to transport water

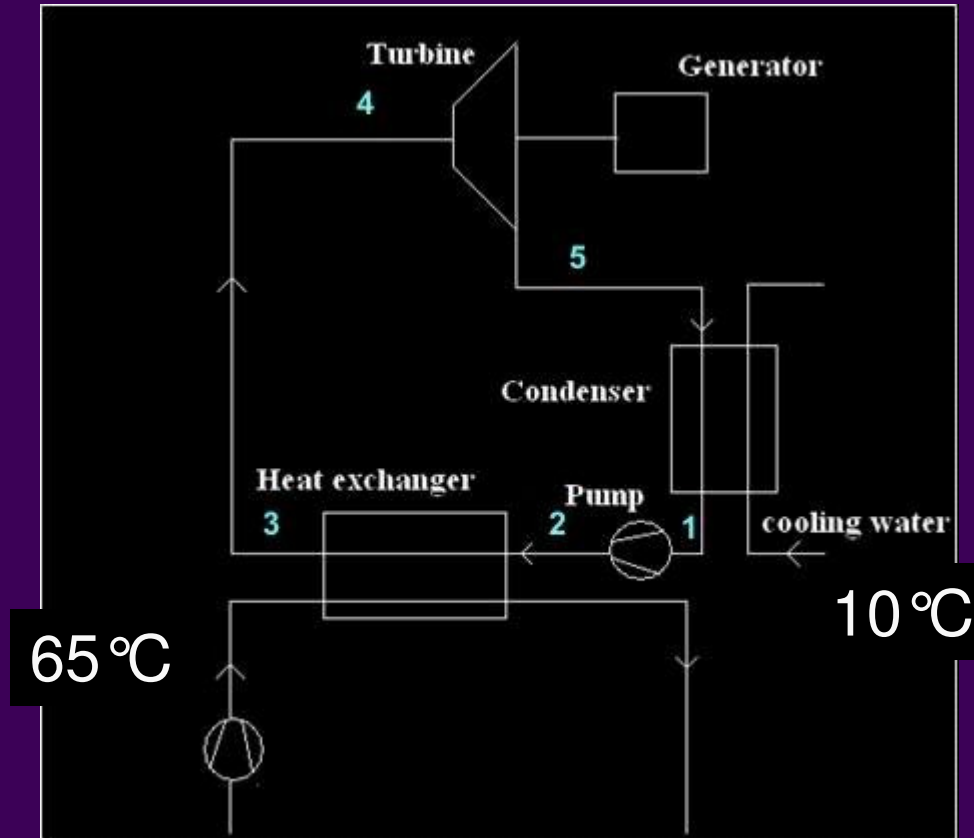
Wet Type Cooling Towers

- Mechanical draft (fan)
- Cool water loop with $\Delta T \sim 10^\circ\text{C}$
- Deliver $>25^\circ\text{C}$
- 40°C condensing temperature
- 30 t/h per MW_e of make-up water
 - *evaporation & blowdown*
- Flash Plants
 - *direct contact condensers*

Dry Type Cooling Towers

- Mechanical draft (fans)
- Deliver ambient temperature air
- 40-50 °C condensing temperature
- No need for make-up water
- Most expensive option:
 - *5-10 times more costs than wet type*
 - *20-50% higher binary plant costs*
- The only option in case of water scarcity or cold climatic extremes

R134a Rankine Cycle Optimization (LOW-BIN project)



using the EASY software code (Evolutionary Algorithm System)
by National Technical University of Athens, ref. <http://velos0.ltt.mech.ntua.gr/EASY>

Modeling the Condenser

Overall heat transfer:

$$U_o = \frac{1}{\frac{A_o}{A_i} \frac{1}{h_i} + \frac{A_o \ln(r_o / r_i)}{2\pi k L} + \frac{1}{h_o}}$$

Laminar condensation
on tubes surface:

$$h_o = 0.725 \left[\frac{\rho(\rho - \rho_v) g h_{fg} k_f^3}{\mu_f d (T_g - T_w)} \right]^{0.25}$$

Turbulent flow in tubes:

$$h_i = \frac{Nu k}{D}$$

$$Nu = 0.023 Re^{0.8} Pr^{0.4}$$

Optimization Variables

variable	min	max
R134a pump discharge pressure P_2 , bar	7,5	12,0
Geothermal water mass flow m_{gr} , kg/s	45	55
R134a mass flow m_{134a} , kg/s	10	20
Geothermal water ΔT_H , °C	10	30
Cooling water ΔT_C , °C	7,5	12,5

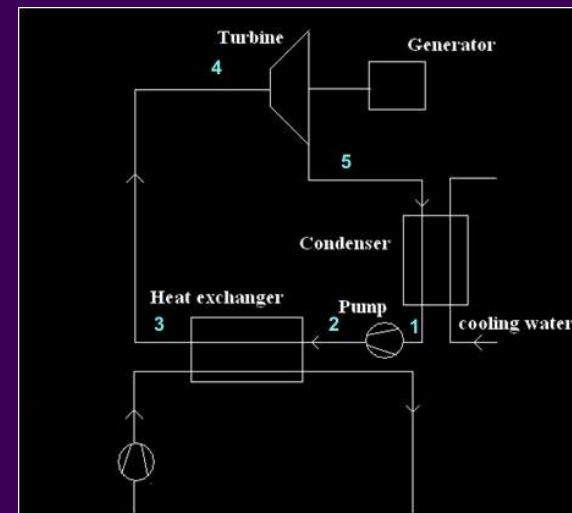
Optimization Objectives

- Maximum conversion efficiency

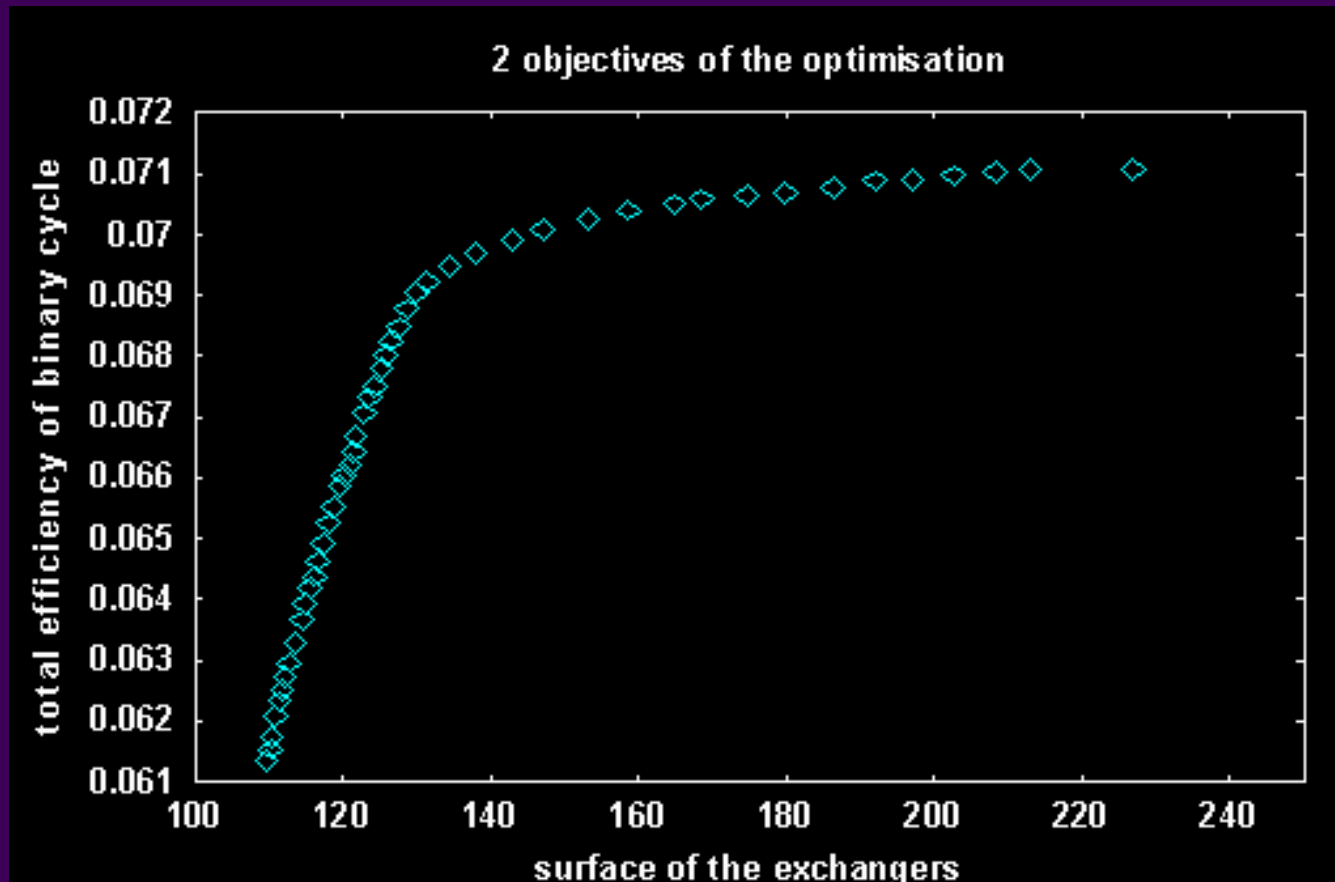
$$\eta_{cycle} = \frac{w_{turbine}}{q_{heatexch}} = \frac{h_4 - h_5}{h_3 - h_2}$$

- Minimum costs

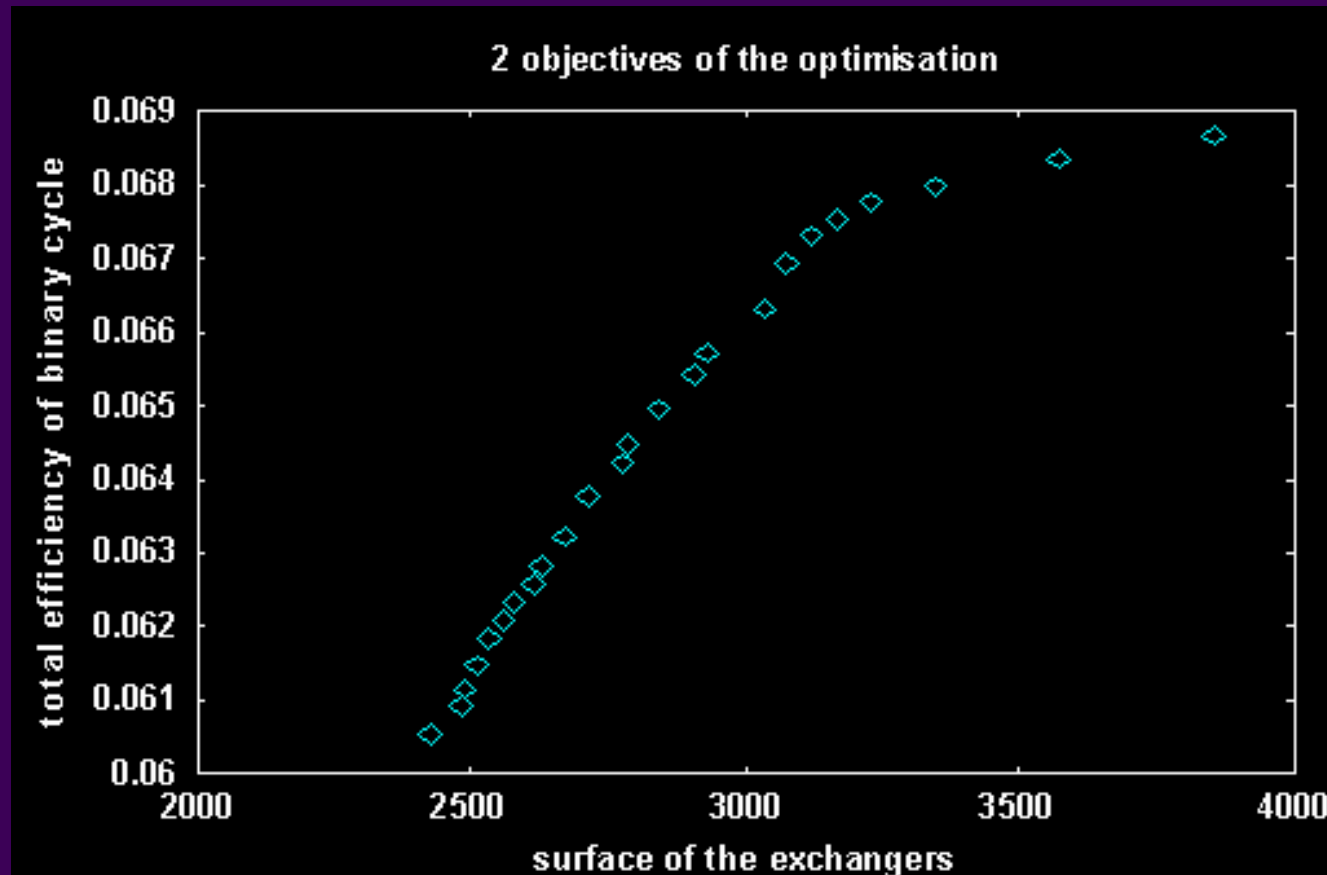
\Rightarrow *minimum heat exchange surface*



Water Cooled Rankine Cycle



Air Cooled Rankine Cycle



Water vs. Air Cooled

variable	Water cooled	Air cooled
$P_{2-R134a}$ (bar)	11	11
m_{gr} (kg/sec)	52,3	53,0
m_{134a} (kg/sec)	17,5	17,5
ΔT_H (°C)	17,5	17,8
ΔT_C (°C)	7,5	7,5
R134a pump power (KW)	13	12
cooling fluid flow (m ³ /h)	403	$3,45 \cdot 10^5$
Overall heat transfer coefficient U	5580	102
Surface of the condenser (m ²)	88	3160
Total H.E. surface (m ²)	138	3230
Conversion Efficiency	6,96 %	6,78 %

Conclusions

- Cooling improves conversion efficiency
- Binary Plants:
Efficiency ↓ , Costs ↑ , Water needs ↓ for:

Cooling with surface water



Wet type cooling towers



Dry type cooling towers